

Designed Cellular Coal

Field of the Invention

5 The present invention relates to cellular coal products formed from coal and to their methods of production and more particularly to such products that are custom manufactured to provide regions and volumes within their structures that exhibit varying strength, density and or porosity characteristics.

Background of the Invention

10 U.S. Patent Application Serial No. 09/453,729, filed December 2,1999 entitled “Cellular Coal Products and Processes” describes coal-based cellular or porous products having a density of preferably between about 0.1g/cm^3 and about 0.8g/cm^3 that are produced by the controlled heating of coal particulate preferably up to 15 1mm in diameter in a “mold” and under a non-oxidizing atmosphere. The porous products produced by these processes, preferably as a net shape or near net shape, can be machined, adhered and otherwise fabricated to produce a wide variety of low cost, low density products, or used in its preformed shape as a filter, heat or 20 electrical insulator etc. Such cellular products have been shown to exhibit compressive strengths of up to about 4000 psi. Impregnation with appropriate materials or the incorporation of various strength improving additives can further increase the compressive, tensile and other properties of these cellular materials.

Further treatment by graphitization yields cellular products that can be used as electrical or heat conductors.

5 The coal-based products described in the foregoing U.S. Patent Application have many potential uses that are supported by their low densities, high strengths, thermal and electrical conductivities and fluid permeabilities, however, many such applications or uses require combinations of such properties in order to provide the desired product. For example, while low density and relatively high strength may be required for a specified use, attachment of the coal-based foam product

10 demonstrating such low density and relatively high strength may require the inclusion of a very high strength region in a portion of the product part to permit the passage of a fastener that will induce areas of high mechanical stress in the area of fastener passage. Similarly, while fluid permeation of the coal-based cellular product may be desired in one direction, it may be necessary to limit or inhibit such

15 fluid permeation in orthogonal directions to achieve directed fluid flow as through a "pipe". It can also be envisioned that a low-density coal-based product part may require the inclusion of high strength regions to provide structural properties in regions thereof that are subjected to elevated directional mechanical stresses that the bulk of the low density material cannot adequately support.

20

Thus, it would be highly desirable to be able to custom design various regions of the coal-based cellular product to support various different strength, thermal and electrical conductivity and fluid permeation properties in the various regions of the

coal-based cellular product. Stated differently, it would be highly desirable to possess the ability to provide coal-base cellular products and parts produced from a single cell forming process that exhibit integral: 1) stiffeners or load paths; 2) directed heat or electrical transfer paths; and 3) directed mass transfer paths.

5

Object of the Invention

It is therefore an object of the present invention to provide a method for the production of coal-based cellular products and parts that exhibit integral, custom designed and varying strength, thermal and electrical conductivity and fluid permeabilities throughout their overall volumes.

10

Summary of the Invention

According to the present invention, coal-based cellular products having integral stiffeners or load paths, directed heat transfer paths and directed mass transfer paths are provided through the placement of coal-based cells of a different size and/or density than those making up the matrix of the product during manufacture. There is also provided a method for the production of coal-based cellular products possessing these characteristics. The method of the present invention utilizes the ability to select and design such properties through the proper selection and control of cell size and density. Such control of cell size and density is in turn achieved through appropriate selection of starting materials, starting material particle size, mold packing and processing parameters.

15

20

Description of the Drawings

5 **Figure 1 is a photomicrograph of a horizontally graded coal-base cellular product.**

Figure 2 is a photomicrograph of a vertically graded coal-based cellular product.

10 **Figure 3 is a photomicrograph of a mixed precursor coal-based cellular product.**

Figure 4 is a photomicrograph of a radially graded coal-based cellular product.

15 **Figure 5 is a photographic mage of a coal-base cellular product incorporating differing cell sizes in the shape of the letter T.**

Figure 6 is a photographic image of a coal-based cellular product
20 **incorporating differing cell sizes in the shape of the letter T.**

Detailed Description

According to the method described in aforementioned U.S. Patent Application Serial No. 09/453,729, a low density, i.e., from about 0.1 to about 1.0g/cm³, and preferably from about 0.2 to about 0.5g/cm³, coal-based cellular product is produced from powdered coal particulate preferably less than about 1mm in diameter by the controlled heating of the powdered coal in a "mold" under a non-oxidizing atmosphere. The starting material coal may include bitumen, anthracite, or even lignite, or blends of these, but is preferably bituminous, agglomerating coals that have been comminuted to an appropriate particle size, preferably to a fine powder below about -60 to -80 mesh. As used herein, the term "coal-based" is meant define that the cellular products described herein are prepared or manufactured by the "controlled swelling" of ground or comminuted coal.

These cellular coal-based products are semi-crystalline or more accurately turbostratically-ordered and largely isotropic i.e., demonstrating physical properties that are approximately equal in all directions, and typically exhibit pore sizes on the order of less than 100μm, although pore sizes of up to 2000μm are possible within the operating parameters of the process described. The thermal conductivities of the cellular coal-based products are generally less than about 1.0 W/m/°K.

Typically, the cellular coal-based products of the present invention demonstrate compressive strengths on the order of from about 2000 to about 4000 psi at densities of from about 0.4 to about 0.5g/cm³.

5 The production method previously described comprises: 1) heating a coal particulate of preferably small i.e., less than about 200 μ m particle size in a "mold" and under a non-oxidizing atmosphere at a heat up rate of from about 1 to about 20°C per minute to a temperature of between about 300 and about 700°C; 2) soaking at a temperature of between about 300 and 700°C for from about 10 minutes up to about 12 hours to form a preform or finished product; and 3) controllably cooling the preform or finished product to a temperature below about 100°C. The non-oxidizing atmosphere may be provided by the introduction of inert or non-oxidizing gas into the "mold" at a pressure of from about 0 psi, i.e., free flowing gas, up to about 500 psi. The inert gas used may be any of the commonly used inert or non-oxidizing gases such as nitrogen, helium, argon, CO₂, etc.

15 It is generally not desirable that the reaction chamber be vented during the heating and soaking operation. The pressure of the chamber and the increasing volatile content therein tends to retard further volatilization while the cellular product sinters at the indicated elevated temperatures. If the furnace is vented during soaking, an insufficient amount of volatile matter may be present to permit inter-particle sintering of the coal particles thus resulting in the formation of a sintered powder as opposed to the desired cellular product.

20 Additional more conventional blowing agents may be added to the particulate prior to expansion to enhance or otherwise modify the pore-forming operation.

09733606 120300

The term “mold”, as used herein is meant to define a device for providing controlled dimensional forming of the expanding coal. Thus, any chamber into which the coal particulate is deposited prior to or during heating and which, upon the coal powder attaining the appropriate expansion temperature, contains and shapes the expanding porous coal to some predetermined configuration such as: a flat sheet; a curved sheet; a shaped object; a building block; a rod; tube or any other desired solid shape can be considered a “mold” for purposes of the present invention. Mold materials include glass and ceramics as well as aluminum and steel. As will be explained more completely below, the selection of mold material and consequently heating/volitization rates can affect cell formation and product properties and is consequently an important consideration in the production of the custom designed foams of the present invention.

As will be apparent to the skilled artisan familiar with pressurized gas release reactions, as the pressure in the reaction vessel increases, from 0 psi to 500 psi, as imposed by the non-oxidizing gas, equilibrium will be shifted and the density of the produced coal-based cellular product will increase as the size of the “bubbles” or pores produced in the expanded coal decreases. Similarly, a low soak temperature of, for example about 400°C will result in a smaller pore or bubble size and consequently a more dense expanded coal than would be achieved with a soak temperature of about 600°C. Further, the heat-up rate will also affect pore size, a faster heat-up rate resulting in a larger pore size and consequently a less dense

expanded coal product than a slow heat-up rate. These phenomenon are, of course, due to the kinetics of the volatile release reactions which are affected, as just described, by the ambient pressure and temperature and the rate at which that temperature is achieved as well as the material composition of the mold. These
5 process variables can be used to custom produce the expanded coals of the present invention in a wide variety of controlled densities, strengths etc.

After expanding the coal particulate as just described, the porous coal product is an open celled material. Several techniques have been developed for
10 “sealing” the surface of the open celled structure to improve, for example, its adhesive and permeability characteristics for further fabrication and assembly of a number of parts or for particular utilities. For example, a layer of a commercially available graphitic adhesive can be coated onto the surface and cured at elevated temperature or allowed to cure at room temperature to provide an adherent skin.

15 After expanding, the porous coal-based preform or product is readily machineable, sawable and otherwise readily fabricated using conventional fabrication techniques.

Subsequent to production of the preform or product as just described, the
20 preform or product may be subjected to carbonization and/or graphitization according to conventional processes to obtain particular properties desirable for specific applications. Activation, for example, by ozone or carbon dioxide, may also be performed, if activation of the coal-based expanded product would be useful in a

final product application such as in filtering of air. Additionally, a variety of additives and structural reinforcers may be added to the coal-based preforms or products either before or after expansion to enhance specific mechanical properties such as fracture strain, fracture toughness and impact resistance. For example, particles, whiskers, fibers, plates, etc. of appropriate carbonaceous or ceramic composition can be incorporated into the porous coal-based preform or product to enhance its mechanical properties.

The open celled, coal-based preforms or products can additionally be impregnated with, for example, petroleum pitch, epoxy resins, phenolic resins or other polymers using a vacuum assisted resin transfer type of process. The incorporation of such additives provides load transfer advantages similar to those demonstrated in carbon composite materials. In effect a 3-D composite is produced that demonstrates enhanced impact resistance and load transfer properties.

The cooling step in the expansion process results in some relatively minor shrinkage on the order of less than about 5% and generally in the range of from about 2% to about 3%. This shrinkage must be accounted for in the production of near net shape preforms or final products of specific dimensions and is readily determinable through trial and error with the particular coal starting material being used. The shrinkage may be further minimized by the addition of some inert solid material such as coke particles, ceramic particles, ground waste from the coal expansion process etc. as is common practice in ceramic fabrication.

Carbonization is conventionally performed by heating the preform or product under an appropriate inert gas at a heat-up rate of less than about 10°C per minute to a temperature of between about 800°C and about 1200°C and soaking for about 1 hour or less. Appropriate inert gases are those described above that are tolerant of these high temperatures. The carbonization process serves to remove all of the non-carbon elements present in the preform or product such as sulfur, oxygen, hydrogen, etc.

Graphitization, commonly involves heating the preform or product either before or after carbonization at heat-up rate of less than about 20°C per minute, preferably from about 1°C to about 5°C per minute, to a temperature of between about 1700°C and about 3000°C in an atmosphere of helium or argon and soaking for a period of less than about one hour. Again, the inert gas may be supplied at a pressure ranging from about 0 psi up to a few atmospheres.

Through previous work performed in connection with above-referenced U.S. Patent Application Serial No. 09/ 453,729 which is hereby incorporated by reference in its entirety, it has been determined that the cell size of coal-base cellular products is largely determined by the particle size of the starting carbonaceous material. Large cells are produced from large particle size precursors while smaller cells are produced from small particle size precursors. Additionally, it has been discovered that density can be graded or varied by both selection of different precursors or

starting materials as well as thermal gradients within the mold. The latter, as will be shown, below can be controlled by the selection of mold materials to accelerate or decelerate heat up and cool down rates.

5 Coals suitable for use in the processes described herein are primarily bituminous coals exhibiting a "swell index" as determined by ASTM standards DD5515-97, "Standard Test Method for the Determination of Swelling Properties of Bituminous Coal" and D720-91 "Standard Test Method for Free Swelling Index of Coal" of between about 3 and about 9 and preferably about 4. Best results are
10 achieved in terms of adequate cell generation to obtain coal-based cellular materials of the proper densities when the bituminous coal demonstrates a Gieseler plasticity value commonly characterized as high, i.e. above about 500DDPM. Such values are determined in accordance with ASTM standard D-2639. Agglomerating
15 bituminous coals, i.e. those containing from about 10 to about 32% by weight volatiles are specifically preferred.

 In the first proposed application of the processes of the present invention, the overall weight of foams for structural applications can be optimized by locating cellular material of high-density or larger cell wall thickness in regions of high
20 stress, while retaining the lower density or more open-celled structure in less stress-critical regions. This approach can also be used to alter mass properties such as centroid movement, moment of inertia, and radius of gyration of a solid body.

For heat transfer, two methods of design are possible. First, regions of high density or larger cell wall thickness can be included to offer greater heat conduction in desired locations or directions with low density cellular material located to insulate or retard heat flow in other locations or directions. Second, in convective or fluid flow applications, regions of larger, more open celled material can be located to allow gas flow and interaction with graphitic cell walls and ligaments, while higher density or more closed cell material can be used to prevent convective flow in other locations or directions. Such a material could find application in heat exchange applications, for example. These latter materials are also applicable to directed mass transfer applications, for example, in catalysis and electrolyte transfer. In these case, coal-based cellular materials can be designed to allow preferential reactant or electrolyte transfer in a given direction(s) to optimize the efficiency of fuel cells, batteries, catalytic and electrochemical processes. Hence, the coal-based cellular products of the present invention provide the integration of a cellular structure demonstrating a particular strength, heat transfer or mass transfer characteristic in a coal-based cellular matrix of a compositionally similar but characteristically dissimilar coal-based cellular structure.

Coal-based cellular materials of this type, hereinafter called “graded materials” are produced by segregating starting materials having different particle size distributions using partitions placed in the mold during loading. The partitions can then be removed prior to heating without material displacement and the different cell sizes thereby segregated in the chosen regions. Alternatively, the

partitions may comprise materials such as paper that are vaporized during the heating operation, or even carbon meshes or fabrics that become incorporated into the structure during heating.

5 Density can be similarly graded by two distinct means; 1) use of different precursors and 2) the proper and controlled application of thermal gradients. In the first method, different starting materials are segregated by partitions in the loading operation as just described. For example, part of the mold can be filled with a high volatile bituminous coal and the balance of the mold filled with a low volatile
10 bituminous coal. In this situation, the mass loss and sintering behavior of the two different starting materials can be quite different resulting in graded density within the structure.

 In the second proposed application of the processes of the present invention,
15 thermal conditions during cell formation are used to create density gradients within the formed article. For example when cell formation is performed in a thermally insulating mold (glass or ceramic, for example) under rapid heat up conditions, volatiles are largely removed from the top or outer surface areas before the interior material reaches temperature. The surface material thus becomes dense due to
20 being pushed upward or outward by the more slowly expanding internal material. A product formed in such a process will have a dense skin and a less dense core. Thermal conditioning can also be used to produce the opposite effect. If a suitable material is rapidly heated to a very high temperature and/or if the mold is made of a

thermally conductive material such as steel or aluminum, the material adjacent to the mold surface devolatilizes quickly and becomes rigid, i.e. cokes and remains more porous, while the internal structure is being formed and cannot "collapse" the outer surface during expansion as in the case of the slow heat up rate process in an
 5 insulating mold just described.

The invention will be better understood when considered in light of the following, non-limiting examples of its implementation.

10

Examples

Example 1

A high volatile bituminous coal was ground and sieved to produce two distinct particle size ranges; 1) that passing through a 60 mesh screen, and 2) that
 15 passing through a 30 mesh screen but not a 35 mesh screen. Equal amounts of both sizes were weighed and poured onto opposite sides of a paper partition that had been placed across the diameter of a circular ceramic mold. After vibrating the mold to achieve proper particle packing, the partition was removed and the mold loaded into a pressure vessel. The mold under nitrogen pressure of 500 psi was
 20 heated to 475°C at a heating rate of 3°C per minute and held at this temperature for seven hours. The resulting cellular product was calcined at 1000°C and then cut to reveal the graded cell structure shown in Figure 1.

Example 2

A high volatile bituminous coal (610 from Pike County, Kentucky) was ground until it passed through an 80 mesh screen, loaded into a steel mold and placed in a pressure vessel containing nitrogen at atmospheric pressure. While this material is known from previous experience to produce a uniform density cellular material when subjected to temperatures between about 425°C and 475°C, it was heated rapidly to 525°C and held at this temperature for seven hours. The resulting structure, showing a low density inner portion and a high density surface is shown in Figure 2.

10 Example 3

A low volatile bituminous coal was ground until all material passed through a 60-mesh screen. Similarly, a high volatile bituminous coal (610 from Pike County, Kentucky) was ground until it passed through an 80-mesh screen. Equal amounts of both precursors were weighed and poured on opposite sides of a paper partition placed across the diameter of a circular ceramic mold. After vibrating the mold to achieve proper packing, the partition was removed and the mold loaded into a pressure vessel containing nitrogen at 500psi. The mold was heated to 475°C at a slow heating rate (2°C per minute) and held at this temperature for seven hours. The resulting cellular material was cut to reveal the graded cellular structure shown in Figure 3.

Example 4

An NMP (n-methyl pyrrolidone) extract of a low volatile bituminous coal was ground until all material passed through a 60-mesh screen. It was loaded into a ceramic mold and heated slowly to a temperature of 475°C and held for seven hours. The exterior material volatilized first and was pushed outward to the mold surface by the expanding interior giving rise to the pronounced "skin-core" structure shown in Figure 4.

Example 5

A high volatile bituminous coal was ground and sieved to produce two distinct particle sizes. The first (1) passed through a 60 mesh screen and the second (2) through a 35 mesh but not a 60 mesh screen. A T-shaped mold was constructed from paper and centered in a cylindrical steel mold. The relative areas of the T and the surrounding mold were used to determine the amounts of each material used. In one case, fraction 1 was loaded into the T and fraction 2 into the surrounding mold. In the second case, fraction 2 was loaded into the T and fraction 1 into the surrounding mold. Both were heated to 475°C at a heating rate of 2°C per minute and held at this temperature for seven hours. The resulting cellular materials were cut to reveal the linearly-graded cell structure shown in Figures 5 and 6 respectively.

20

There have thus been described, coal-based cellular products that can be custom designed to have integral stiffeners or load paths, directed heat transfer paths, and/or directed mass transfer paths and methods for their production. Such

5

17